

## Sample Boiler Calculations:

### 1. Convert actual steam rating into From and At 100 C

Steam capacity from and at 100 C (212 F) is equivalent steam capacity if operating conditions are reduced to atmospheric pressure.

$$\begin{aligned}\text{Steam capacity} &= 8000 \text{ kg/hr at } 10.5 \text{ kg/cm}^2 \text{ saturated} \\ \text{Feed water inlet} &= 30 \text{ C} \\ \text{Heat load} &= 8000 (664-30) \text{ Kcal/hr} \\ &= 5.072\text{e}06 \text{ Kcal/hr} = 20.127\text{e}06 \text{ btu/hr} = \\ &5.8976 \text{ MW}\end{aligned}$$

$$\begin{aligned}\text{where Sat steam enthalpy} &= 664 \text{ Kcal/kg} \\ \text{Inlet water enthalpy} &= 30 \text{ Kcal/kg} \\ \text{Steam enthalpy at } 100\text{C and } 1 \text{ atm pressure} &= 540 \\ &\text{Kcal/kg}\end{aligned}$$

$$\begin{aligned}\text{Therefore, steam capacity F\&A } 100 \text{ C} &= 5.072\text{e}06/540 \\ &= 9392 \text{ Kg/hr}\end{aligned}$$

### 2. Heat Duty Calculations :

Let us calculate heat duty of a boiler generating 50,000 kg/hr at 65 bar and 485 C  
Water inlet temperature = 105 C

Steam & water properties:

Superheated steam enthalpy at 65 bar & 485 C = 808 Kcal/kg  
Saturated water enthalpy = 295 Kcal/kg

$$\begin{aligned}\text{Heat Duty} &= 50000 \times (808 - 105) \\ &= 35.15\text{e}06 \text{ Kcal/hr (139.48e}06 \text{ Btu/hr or 40.87 MW)}\end{aligned}$$

Usually 1 – 3% of the water flow is used for blowdown.

$$\begin{aligned}\text{Considering } 2\% \text{ blow down, heat in blowdown water} &= 50000 \times 0.02 \times \\ (295 - 105) & \\ &= 0.19\text{e}06\end{aligned}$$

kcal/hr

$$\begin{aligned}\text{Total heat duty} &= (35.15 + 0.19) \text{ e}06 = 35.34\text{e}06 \text{ kcal/hr} \\ &= 140.24\text{e}06 \text{ Btu/hr} = 41.09\end{aligned}$$

MW

In case of Hot water generator or hot water boiler,

Heat duty = Water flow x Cp of water x Temp gain

For example, 200,000 kg/hr of water is heated from 70 to 90 degC,

$$\begin{aligned}\text{Heat Load} &= 200,000 \times 1 \times (90-70) \\ &= 4.0e06 \text{ Kcal/hr} \\ &= 15.873e06 \text{ Btu/hr or } 4.651 \text{ MW}\end{aligned}$$

### 3. Heat Transfer calculations:

Over all heat transfer coefficient,

$$U_o = 1 / (1/H_o + R_m + 1/H_i * (\text{TubeOD}/\text{TubeID}) + R_o + R_i * (\text{TubeOD}/\text{TubeID}))$$

Where  $H_o$  = Outside heat transfer coefficient  
 $H_i$  = Inside heat transfer coefficient  
 $R_m$  = tube metal resistance  
 $R_o$  = Fouling resistance on outside tubes  
 $R_i$  = Fouling resistance on inside tubes

Inside Heat Transfer coefficient can be calculated using the following correlation :

$$Nu_{\text{Inside}} = 0.023 * (Re_{\text{Inside}}^{0.8}) * (Pr_{\text{Inside}}^{0.4})$$

Where  $Nu_{\text{Inside}} = H_i \times \text{TubeID} / \text{Gas Cond}$

Outside heat transfer coefficient during boiling is very high and so resistance offered is negligibly small. There are many correlations available to predict  $H_o$ , but  $H_o$  can be safely assumed to be about 10000 Kcal/hr/m<sup>2</sup>/C.